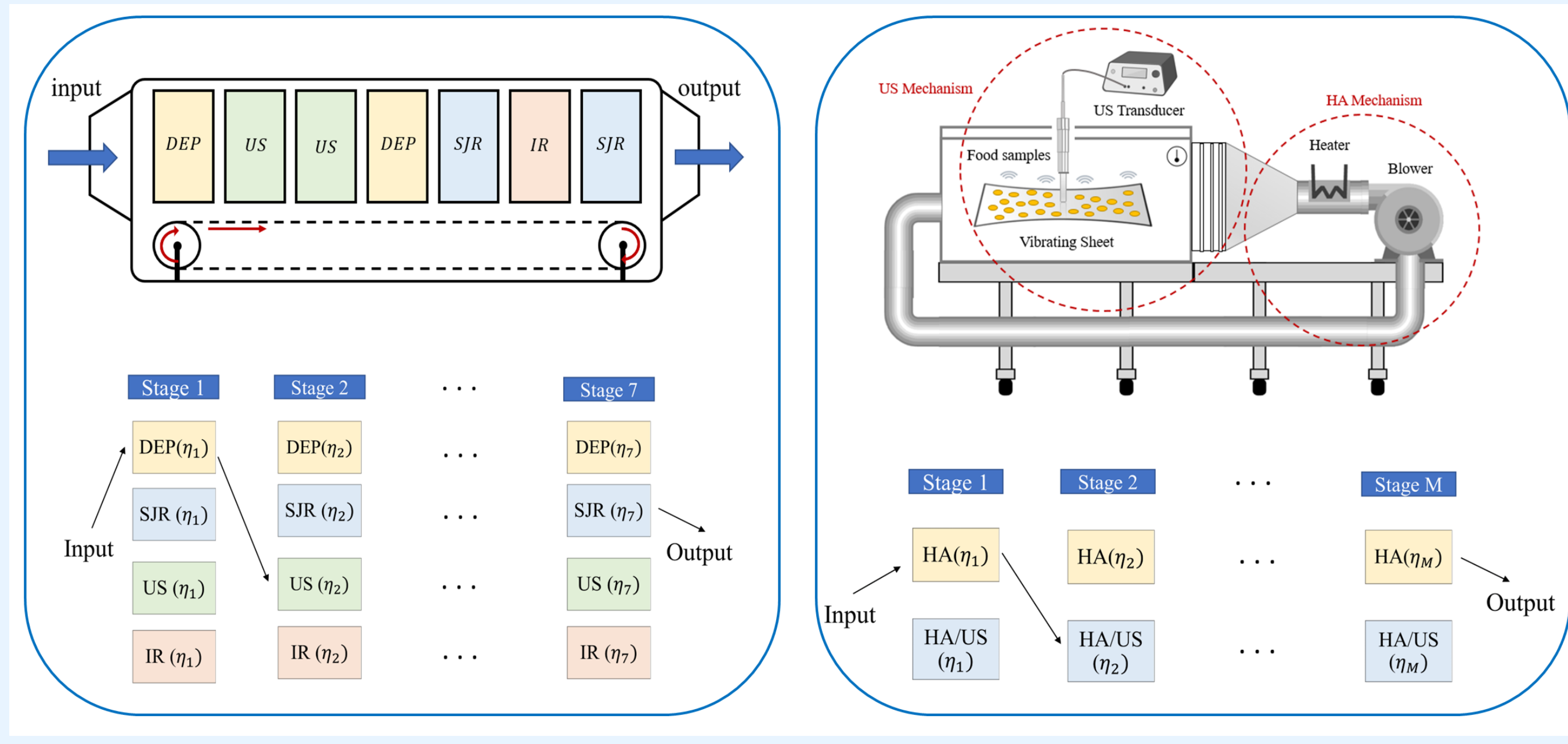


Motivation

- Industrial drying accounts for a significant proportion of energy consumption in manufacturing (12% or 1.2 quads/year), and adopting efficient controls and drying technologies could reduce this by up to 40% (0.5 quads/year), resulting in cost savings of up to \$8 billion per year while also impacting food product quality
- Adopting a modular approach to industrial drying by combining multiple drying technologies with optimal sequencing and control parameters for each can lead to cost-efficient and high-performing drying
- The problem of *simultaneously* determining the optimal a) process configuration and b) operating conditions of each sub-process is NP-hard, with a non-convex cost surface containing multiple poor local minima



Problem Formulation

General Formulation

$$\min_{\{\eta_k\}, \nu(\omega)} \sum_{\omega \in \Omega} \nu(\omega) D(\omega, \eta_1, \dots, \eta_M),$$

$$\text{subject to: } \sum_{\omega \in \Omega} \nu(\omega) = 1, \nu(\omega) \in \{0, 1\}, \eta_k \in H(\gamma_k) \quad \forall 1 \leq k \leq M,$$

- $\omega := (\gamma_1, \gamma_2, \dots, \gamma_M)$, $\gamma_k \in \Gamma_k$: Sub-processes' sequence
- $\Gamma_k := \{f_{k1}, \dots, f_{kL_k}\}$: Set of permissible sub-processes for k -th stage
- $\eta_k \in H(\gamma_k)$: Control parameters of the k -th sub-process

UIUC Hot-Air/Ultrasound Batch-process Testbed

Decision Variables:

$$\gamma_k = \begin{cases} 1 & \text{HA/US} \\ 0 & \text{HA} \end{cases}, \eta_k = \begin{bmatrix} t_k \\ T_k \end{bmatrix} \in U := \left\{ \begin{bmatrix} t \\ T \end{bmatrix} \in \mathbb{R}^2 : t \geq 2, T \in [30, 70]^\circ\text{C} \right\}$$

Dynamics: Moisture content kinetics

$$x_k^{(\omega)} = f_{\gamma_k}(x_{k-1}^{(\omega)}, \eta_k), \quad x_0^{(\omega)} : \text{initial moisture content}$$

Process Cost: Energy consumption + Terminal moisture content cost

$$D(\omega, \eta_1, \dots, \eta_M) = \sum_{k=1}^M \underbrace{(\alpha \eta_{air} c_p (T_k - T_0))}_{\text{HA}} + \underbrace{\gamma_k P_{US}}_{\text{US}} t_k + \underbrace{G(x_M^{(\omega)}, x_d)}_{\text{Terminal Penalty}}$$

Problem solution

- Maximum entropy principle (MEP):

$$\max_{p(\omega)} H := - \sum_{\omega \in \Omega} p(\omega) \log(p(\omega))$$

$$\text{subject to: } \bar{D} := \sum_{\omega \in \Omega} p(\omega) D(\omega, \eta_1, \dots, \eta_M) = D_0, \quad \sum_{\omega \in \Omega} p(\omega) = 1 \quad (1)$$

- Free energy (F): The Lagrangian of the above problem

$$F := \bar{D} - \frac{1}{\beta} H + \mu (\sum_{\omega \in \Omega} p(\omega) - 1)$$

$$\begin{cases} \beta \rightarrow 0 : & H \text{ dominates} \Rightarrow F \text{ is convex} \\ \beta \rightarrow \infty : & D \text{ dominates} \Rightarrow F \approx D \end{cases}$$

The most unbiased probability distribution over the space of all sequences solves (1), which is obtained by Gibbs' distribution.

$$\frac{\partial F}{\partial p} = 0 \Rightarrow p^*(\omega) = \frac{\exp(-\beta D(\omega, \eta_1, \dots, \eta_M))}{\sum_{\omega' \in \Omega} \exp(-\beta D(\omega', \eta_1, \dots, \eta_M))}$$

$$\Rightarrow F^* = \min_{p(\omega)} F = -\frac{1}{\beta} \log \sum_{\omega \in \Omega} \exp(-\beta D(\omega, \eta_1, \dots, \eta_M))$$

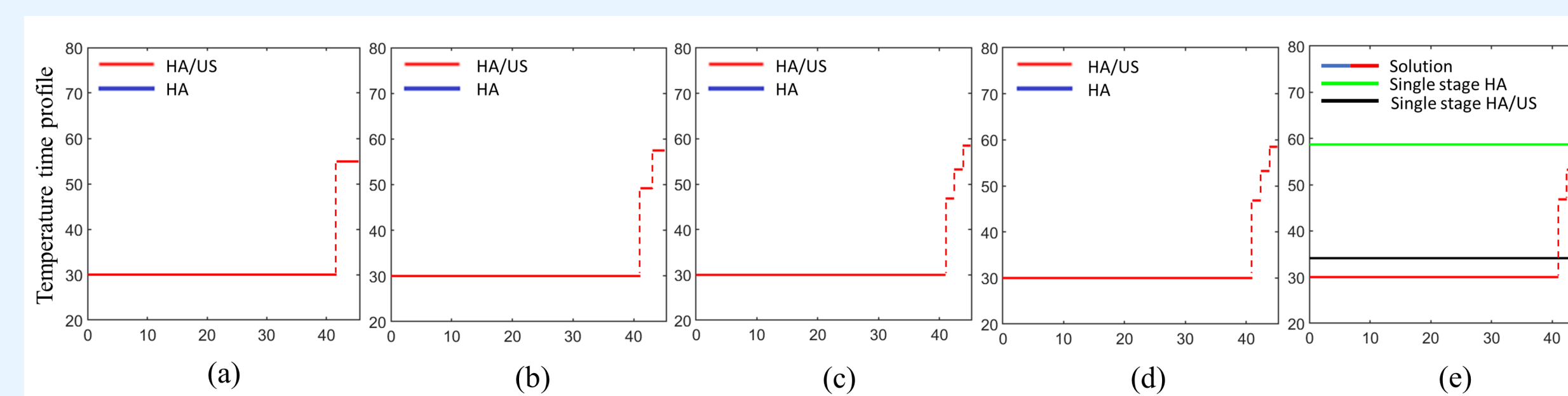
Thus, the following are the three main steps of the algorithm:

- Updating path probabilities: $p(\omega) \leftarrow p^*(\omega) \quad \forall \omega \in \Omega$
- Updating control parameters: $\{\eta_k\} \leftarrow \arg \min_{\{\eta_k \in U\}} F^*$
- Increase β

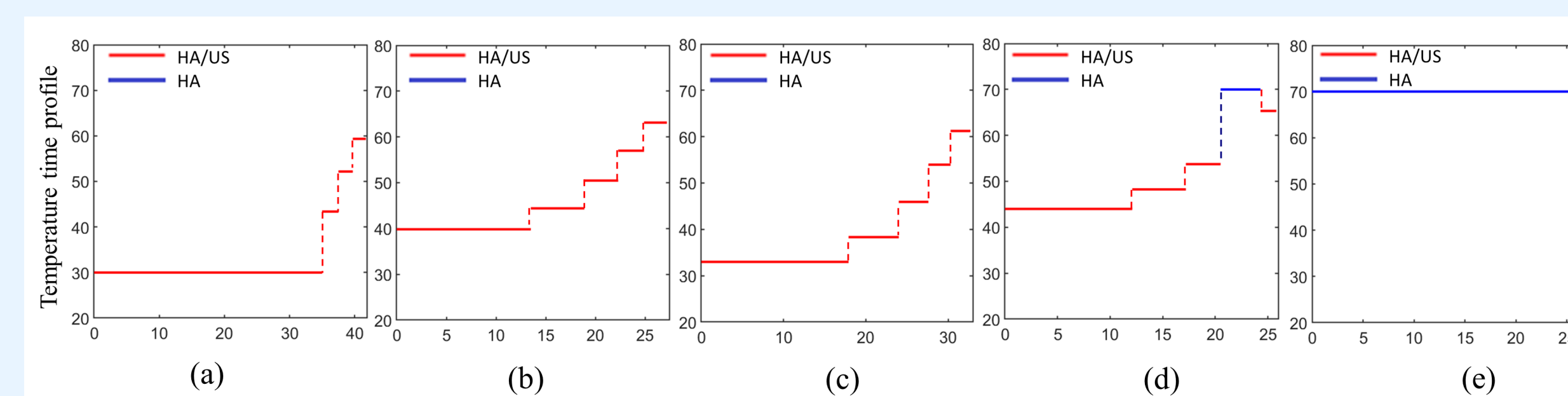
- $\lim_{\beta \rightarrow \infty} p(\omega)$ converges to zero for all non-optimal paths, while it converges to one for the optimal path

Results

- Varying the permissible number of stages (M): Results are shown for $M = 2, 3, 4, 5$. For $M \geq 4$, the total energy consumption is reduced by **63.19%** compared to the optimal single-stage HA, and **12.09%** compared to the optimal single-stage HA/US. Going beyond $M = 4$ does not significantly affect the cost.

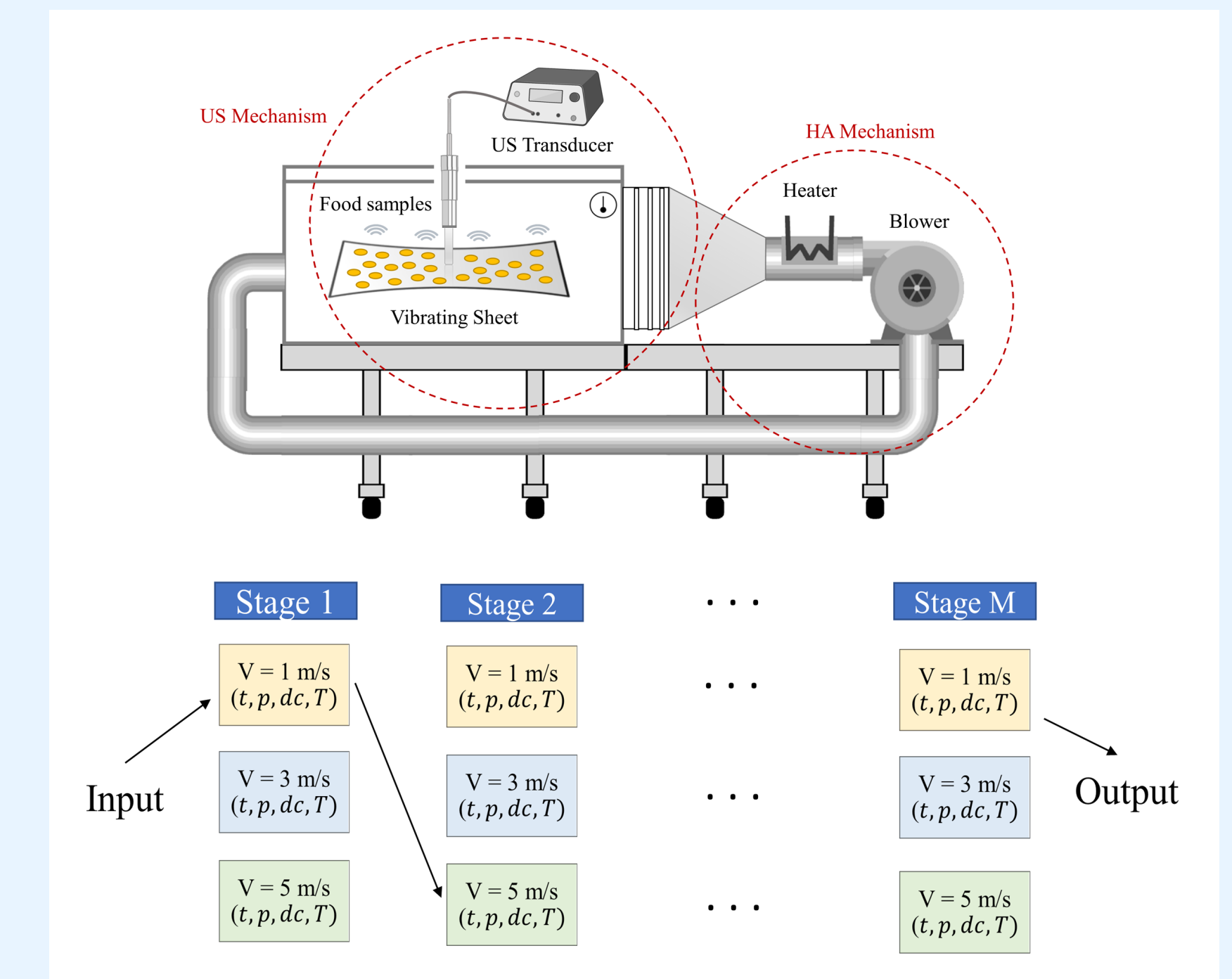


- Varying the relative weight of HA process (α): Decreasing α from 0.2 to 0.04 \rightarrow Increase the cost on the US mechanism. The solutions achieved **9.95%**, **5.75%**, **3.62%**, and **2.08%** improvement compared to the most efficient single-stage processes, respectively.

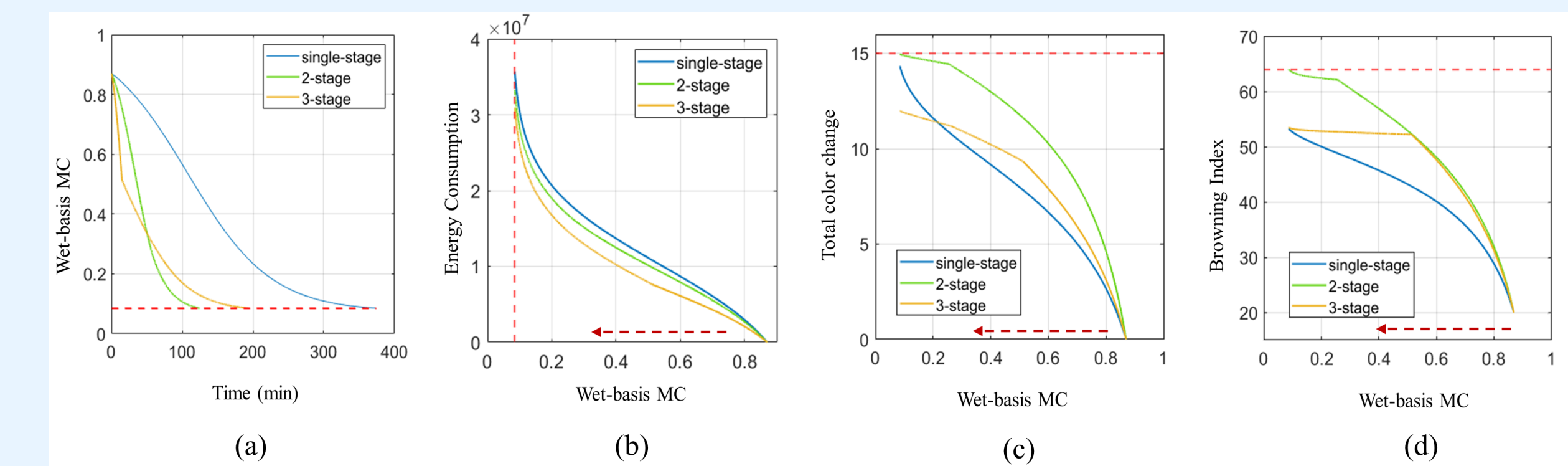


Extension to Mixed-integer Dynamic Optimization

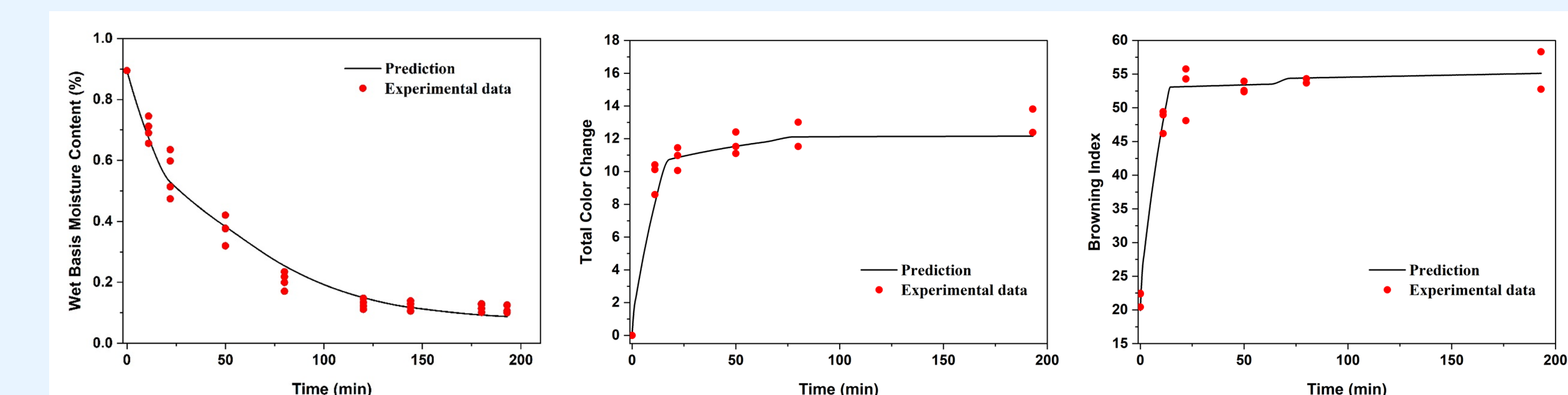
- Problem formulation: 1) Air velocity (V) is discrete, 2) Air temperature (T), US power (p), and US duty cycle (dc) are continuous.



- Results: **13.2%** improvement compared to the optimal single-stage process that satisfies final product constraints on moisture content, total color change, and browning index.



- Validation: Validating the optimal solution with actual experiments.



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